

Modeling Flow Fields in Stirred Tanks

Reacting Flows – Homework 4

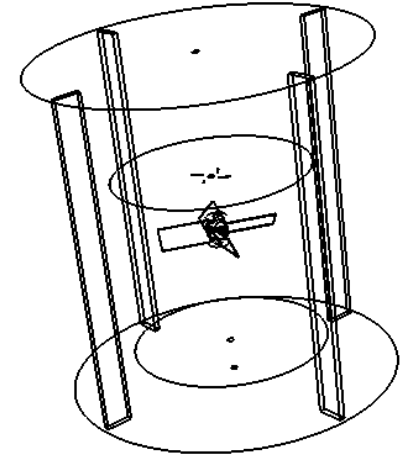
Instructor: André Bakker

Homework assignment

- The purpose of this homework assignment is to calculate a time averaged flow field in a stirred tank.
- Students will be provided with the computational mesh for one of the following cases:
 - Pitched blade turbine
 - HE-3 impeller
 - Rushton turbine
- Assignment:
 - Calculate the flow field at two Reynolds numbers: $Re=10$ and $Re=10,000$. Use the moving reference frame (MRF) impeller model.
 - Calculate the power number and pumping/flow number for both Reynolds numbers. Compare these with data from the literature (e.g. from <http://www.postmixing.com/mixing%20forum/impellers/impellers.htm>)
 - Qualitatively compare the flow predicted with flow fields presented in the literature.
 - Provide results and interpretation in either a PPT or DOC file.
 - Provide final FLUENT case and data files.
- Note: students who already have significant experience with such flow field predictions may propose an alternative assignment to the instructor.

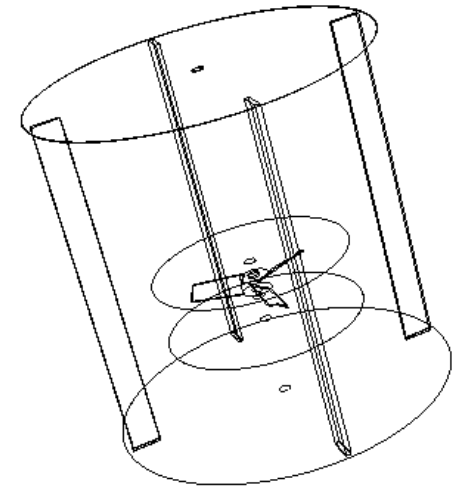
Pitched blade turbine

- Filename: pbt.msh.gz
- Specifications:
 - $T=Z=H=0.292$ m
 - $D/T=0.35$
 - $C/T=0.44$ (bottom impeller blade to bottom vessel)
- Setup hints:
 - Define | Grid Interfaces | interface-inner & interface-outer
 - “fluid-impeller” is fluid region. Motion type=moving reference frame. Rotation-axis origin (0,0,0). Rotation-axis direction (1,0,0). Positive angular velocity will give clockwise rotation seen from the top of the vessel and impeller will pump down.
- Post-processing hints:
 - The axial (x-direction) extents of the impeller blade are from (0.15058 to 0.16542)
 - The radial extents of the impeller blades are from (0.008689 to 0.05154)
- Suggestion for reference:
 - The laminar and turbulent flow pattern of a pitched blade turbine. Bakker et al. 1996.



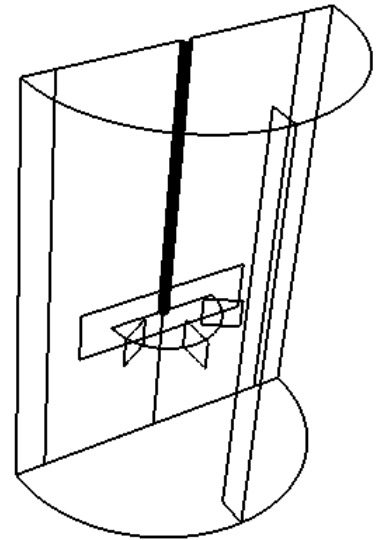
HE-3 impeller

- Filename: he3.msh.gz
- Specifications:
 - $T=Z=H=0.292$ m
 - $D/T=0.394$
 - $C/T=0.33$ (bottom impeller blade to bottom vessel)
- Setup hints:
 - Define | Grid Interfaces | interface-13 & interface-5
 - “fluid-impeller” is fluid region. Motion type=moving reference frame. Rotation-axis origin (0,0,0). Rotation-axis direction (1,0,0). Positive angular velocity will give clockwise rotation seen from the top of the vessel and impeller will pump down.
- Post-processing hints:
 - The axial (x-direction) extents of the impeller blade are from (0.183562 to 0.195494)
 - The radial extents of the impeller blades are from (0.01257 to 0.05759)
- Suggestion for reference:
 - Ward. 1995. DPIV investigation of flow pattern instabilities of axial flow impellers.



Rushton impeller

- Filename: rushton.msh.gz
- Specifications:
 - $T=0.31\text{m}$
 - $Z=H=0.42\text{m}$
 - $D/T=0.4838$
 - $C/T=0.40$ (bottom impeller blade to bottom vessel)
- Setup hints:
 - No grid interfaces. The mesh was created with the two fluid zones connected.
 - “fluid-impeller” is fluid region. Motion type=moving reference frame. Rotation-axis origin $(0,0,0)$. Rotation-axis direction $(0,-1,0)$. Positive angular velocity will give clockwise rotation seen from the top of the vessel.
 - For “fluid”, motion type=stationary. But do specify rotation-axis origin $(0,0,0)$ and rotation-axis direction $(0,-1,0)$. This is necessary for the definition of the rotationally periodic boundary conditions.
 - This mesh is for half a vessel. Need to set up rotationally periodic boundaries. After specifying rotation axes for the two fluid zones, from the text interface:
 - Define boundary-conditions modify-zones make-periodic
 - periodic11 periodic12 yes yes
 - Define boundary-conditions modify-zones make-periodic
 - periodic21 periodic22 yes yes
- Post-processing hints:
 - The axial (y-direction) extents of the impeller blade are from $(0.125$ to $0.155)$
 - The radial extents of the impeller blades are from $(0.0375$ to $0.0075)$
- Suggestion for reference: Computation of flow fields and complex reaction yield. Middleton et al. 1986.



Rushton impeller – more difficult

- Review the paper titled:
 - Investigation of laminar flow in a stirred vessel at low Reynolds numbers.
 - Rice M., Hall J., Papadakis G., Yianneskis M. Chemical Engineering Science 61 (2006) 2762-2770.
- Use the Rushton mesh to calculate the flow field at $Re=1$, 10, and 28, as in the paper.
- Compare the results with Rice et al.
- Notice that the impeller off-bottom clearance is different, and comment on how that may have affected the comparison.